



Theoretical prediction of KF-RbF-CsF-BeF₂ system: phase diagrams calculation and ab initio molecular dynamics

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Abstract

Thermodynamic optimization of the AF-BeF₂ (A = K, Rb, and Cs), KF-CsF, and RbF-CsF systems was performed within the framework of phase diagrams calculation. The model parameters were optimized based on experimental data and theoretically calculated values. The results show that the thermodynamically calculated values for the AF-BeF₂ (A = K, Rb, and Cs), KF-CsF, and RbF-CsF systems agree well with the experimental data. Next, a set of reliable and self-consistent thermodynamic databases was built, and the liquidus projections and invariant points of the sub-ternary systems of the KF-RbF-CsF-BeF₂ system were calculated. Furthermore, the melting temperature with the corresponding composition was predicted using the phase diagrams calculation technique, and the radial distribution functions, coordination numbers, angular distribution functions, and diffusion coefficients of the quaternary KF-RbF-CsF-BeF₂ system were calculated using ab initio molecular dynamics. The results show that the quaternary KF-RbF-CsF-BeF₂ system with the proportion 3.50–28.92–21.78–45.80 mol% or 1.80–35.42–52.40–10.38 mol% is one of the most promising candidate coolants for molten salt reactors in terms of thermodynamics and kinetics. This work provides direct guidelines for the screening and optimization of molten salts in the nuclear energy field.

Keywords Molten salt · KF-RbF-CsF-BeF₂ · Calculation of phase diagrams · Ab initio molecular dynamics

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1 Introduction

Molten salt reactors (MSRs) are the only liquid fuel reactors among the Generation IV nuclear reactors, where the fissile and fertile fluorides (i.e., UF₄, ThF₄, and PuF₃) are dissolved into the molten fluoride salt [1–3]. MSRs have received increasing attention worldwide owing to their significant advantages, such as good neutron economy, less nuclear waste, no water cooling, online post-processing of fission products, and low pressure at high temperature [4–8]. Molten fluoride salt is used as a nuclear fuel and heat transfer fluid medium because of its good neutron properties and excellent thermophysical properties, which play a critical role in the design of nuclear cores, thermal hydraulic calculations, nuclear reactor safety analysis, and the entire operation of nuclear reactors [9–13]. Relevant fluoride salts, which are essential for the design, research, and development of heat transfer media for MSRs must be explored thoroughly.

Molten BeF₂-based salt is considered one of the most promising heat transfer media and nuclear fuel salt carriers

for MSRs due to its favorable thermal neutron-capture cross-section (< 1 barn) and thermophysical properties [14–17]. LiF-BeF₂ is the classic coolant and nuclear fuel medium for the MSRs at Shanghai Institute of Applied Physics in China [18] and Oak Ridge National Laboratory (ORNL) in the U.S. [19]. The LiF-BeF₂ system has been extensively investigated by many researchers. The phase diagram information of the LiF-BeF₂ system was first determined through thermal analysis and thermal gradient quenching by Roy et al. [20], and Moore et al. [21]. Later, the liquidus of the LiF-BeF₂ phase diagram with a 0.12–0.58 mol fraction of BeF₂ was again measured through the electromotive force method by Romberger et al. [22]. The thermochemical properties (i.e., the activity coefficient [23] and mixing enthalpy of the liquid phase [24]) of the LiF-BeF₂ system were experimentally investigated using the electromotive force and single-unit microcalorimeter methods, respectively. The LiF-BeF₂ system was first optimized using Redlich–Kister polynomials by Meer et al. [25], and the thermophysical properties (i.e., the melting point [26], specific heat capacity [17, 27], density [17, 28], viscosity [28–31], vapor pressure [32], thermal conductivity [10], and local structure [33–36]) have been thoroughly studied by performing experimental measurements and theoretical calculations. Compared with the LiF-BeF₂ system, the NaF-BeF₂ system has not been reported on as thoroughly. The phase diagram of the NaF-BeF₂ system was measured based on the differential thermal analysis techniques, high-temperature X-ray diffraction, and the quenching method by Roy et al. [37]. The thermodynamic database of the NaF-BeF₂ system was later built based on the substitutional solution model by Wu et al. [38]. Only limited experimental data regarding the properties of NaF-BeF₂ (i.e., the melting point [10], density [39], viscosity [39], specific heat capacity [17], vapor pressure [40], activity coefficient [41], and local structure [42]) have been reported. The thermophysical properties of the NaF-BeF₂ system were solely calculated using first-principles molecular dynamics by Liu et al. [43]. For the KF-BeF₂ system, limited thermodynamic property information has been obtained [17, 21, 44, 45]. Only the phase equilibria information [21, 46] and a few thermophysical properties [39] for the RbF-BeF₂ system have been experimentally determined, and only the experimental phase diagram of the CsF-BeF₂ system has been determined by thermal analysis [47]. Until now, little other experimental or theoretical information about the AF-BeF₂ (A = K, Rb, and Cs) system has been available, although this information is foundational for the design and operation of processes utilizing molten fluoride salts. Studying the thermodynamic characteristics of the AF-BeF₂ (A = K, Rb, and Cs) system only through experimental measurements is also challenging owing to the difficulty and uncertainty of high-temperature experiments with highly toxic BeF₂. Calculation of phase diagrams (CALPHAD) is one of the

most effective techniques for studying the phase equilibria behavior of multi-component systems based on minimal experimental data. Due to its high accuracy and universality, *ab initio* molecular dynamics (AIMD) is a powerful tool for investigating the interionic forces, local structures, and physio-chemical properties of multi-component systems and has been successfully applied to the LiF-BeF₂ [48–50], NaF-BeF₂ [43, 51], and KF-NaF-AlF₃ [52] systems, among others. In the present work, phase diagrams calculations and AIMD were employed to investigate the thermodynamic and kinetics characteristics of the quaternary KF-RbF-CsF-BeF₂ system.

The thermodynamic calculations for the KF-BeF₂, RbF-BeF₂, CsF-BeF₂, KF-CsF, and RbF-CsF systems were performed using the CALPHAD technique based on experimental data and theoretically calculated values. A substitutional solution model was used to depict the liquid and solid solution phases, and compound energy formalism was employed to describe the intermediate phases, i.e., ABeF₃, A₂BeF₄, A₃BeF₅, and ABe₂F₅ (A = K, Rb, and Cs). The results showed that the thermodynamically calculated values for the KF-BeF₂, RbF-BeF₂, CsF-BeF₂, KF-CsF, and RbF-CsF systems agreed well with the experimental data. Finally, a set of self-consistent and reliable thermodynamic databases was obtained. Additionally, the liquidus projection and invariant points of the corresponding ternary systems of the KF-RbF-CsF-BeF₂ system were calculated. Furthermore, the melting temperatures with the corresponding compositions, radial distribution functions (RDFs), coordination numbers (CNs), angular distribution functions (ADFs), and diffusion coefficients of the quaternary KF-RbF-CsF-BeF₂ system were calculated using AIMD. The results showed that the quaternary KF-RbF-CsF-BeF₂ (3.50–28.92–21.78–45.80 mol% or 1.80–35.42–52.40–10.38 mol%) system is one of the most promising candidate coolants for MSRs in terms of thermodynamics and kinetics. The thermodynamic parameters of the KF-BeF₂, RbF-BeF₂, CsF-BeF₂, KF-CsF, and RbF-CsF systems were firstly built using the CALPHAD technique. The kinetic characteristics of the quaternary KF-RbF-CsF-BeF₂ (3.50–28.92–21.78–45.80 mol% or 1.80–35.42–52.40–10.38 mol%) system were also first obtained in this study using AIMD. These are important fundamentals for thoroughly exploring heat transfer media and nuclear fuel carriers for MSRs. This work provides guidelines for the screening and optimization of molten salts in the nuclear energy field.

2 Literature evaluation

2.1 KF-BeF₂ system

The phase equilibrium information of the KF-BeF₂ system has been reported by three groups of investigators using thermal analysis. The experimental phase diagram of the KF-BeF₂ system was first established by Borzenkova et al. [44]. Four intermediate phases—K₃BeF₅, K₂BeF₄, KBeF₃, and KBe₂F₅—were detected in the KF-BeF₂ system, where only three compounds—K₃BeF₅, K₂BeF₄, and KBeF₃—were stable from room temperature to the melting temperature, whereas KBe₂F₅ was decomposed into KBeF₃ and BeF₂ at 278.0 °C. Afterwards, the KF-BeF₂ system was experimentally determined by Moore et al. [21] at ORNL. The four compounds were again discovered, where K₃BeF₅, K₂BeF₄, and KBe₂F₅ were melted congruently at 740.0 °C, 787.0 °C and 353.0 °C, whereas KBeF₃ was melted incongruently at 405.5 °C; these findings are substantially different from those of Borzenkova et al. [44]. Thus, four eutectic reactions (Liquid $\xrightarrow{720.0^{\circ}\text{C}}$ KF + K₃BeF₅, Liquid $\xrightarrow{730.0^{\circ}\text{C}}$ K₃BeF₅ + K₂BeF₄, Liquid $\xrightarrow{330.0^{\circ}\text{C}}$ KBeF₃ + KBe₂F₅, and Liquid $\xrightarrow{323.0^{\circ}\text{C}}$ KBe₂F₅ + BeF₂) and one peritectic reaction (Liquid + K₂BeF₄ $\xrightarrow{390.0^{\circ}\text{C}}$ KBeF₃) occurred in the KF-BeF₂ system. Novoselova et al. [45] later measured the phase diagram of the KF-BeF₂ system, determining that K₃BeF₅ was incongruently melted at 740.0 °C with a peritectic composition of 0.25 mol BeF₂. Naturally, the KF-BeF₂ system reported by Novoselova et al. is characterized by three eutectic reactions (Liquid $\xrightarrow{700.0^{\circ}\text{C}}$ KF + K₃BeF₅, Liquid $\xrightarrow{327.0^{\circ}\text{C}}$ KBeF₃ + KBe₂F₅, and Liquid $\xrightarrow{346.0^{\circ}\text{C}}$ KBe₂F₅ + BeF₂) and two peritectic reactions (Liquid + K₂BeF₄ $\xrightarrow{740.3^{\circ}\text{C}}$ K₃BeF₅ and Liquid + K₂BeF₄ $\xrightarrow{405.5^{\circ}\text{C}}$ KBeF₃). To date, thermochemical data and thermodynamic parameters for the KF-BeF₂ system are still rare. Herein, the KF-BeF₂ system was thermodynamically optimized through the substitutional solution model in terms of the relatively accurate experimental data from Moore et al. [21].

2.2 RbF-BeF₂ system

A phase diagram of the RbF-BeF₂ system was constructed by two groups of investigators using thermal analysis. Grebenshchikov [46] first established the entire phase diagram of the RbF-BeF₂ system, in which four intermediate phases—Rb₂BeF₄, Rb₃Be₂F₇, RbBeF₃ and RbBe₂F₅—were

detected. Three compounds—Rb₂BeF₄, RbBeF₃, and RbBe₂F₅—were stable and congruently melted separately at 792.0 °C, 464.0 °C, and 451.0 °C, whereas Rb₃Be₂F₇ was unstable and decomposed to Rb₂BeF₄ and RbBeF₃ when the temperature was higher than 423.5 °C. In addition, Rb₂BeF₄ and RbBe₂F₅ are not simple stoichiometric compounds and have a certain solid solubility. Eventually, four eutectic reactions (Liquid $\xrightarrow{689.0^{\circ}\text{C}}$ RbF + Rb₂BeF₄, Liquid $\xrightarrow{461.0^{\circ}\text{C}}$ Rb₂BeF₄ + RbBeF₃, Liquid $\xrightarrow{394.0^{\circ}\text{C}}$ RbBeF₃ + RbBe₂F₅, and Liquid $\xrightarrow{424.0^{\circ}\text{C}}$ RbBe₂F₅ + BeF₂) were formed for the RbF-BeF₂ system. Subsequently, Moore et al. [21] reported the phase equilibrium information of the RbF-BeF₂ system and discovered four intermediate phases: Rb₃BeF₅, Rb₂BeF₄, RbBeF₃, and RbBe₂F₅. The presence of Rb₃BeF₅ versus Rb₃Be₂F₇ was the biggest difference between the works of Grebenshchikov and Moore et al. Moreover, the intermediate compounds Rb₃BeF₅, Rb₂BeF₄, and RbBe₂F₅ melted congruently, whereas RbBeF₃ melted incongruently. Consequently, four eutectic reactions (Liquid $\xrightarrow{675.0^{\circ}\text{C}}$ RbF + Rb₃BeF₅, Liquid $\xrightarrow{720.0^{\circ}\text{C}}$ Rb₂BeF₄ + Rb₃BeF₅, Liquid $\xrightarrow{383.0^{\circ}\text{C}}$ RbBeF₃ + RbBe₂F₅, and Liquid $\xrightarrow{397.0^{\circ}\text{C}}$ RbBeF₃ + BeF₂) and one peritectic reaction (Liquid + Rb₂BeF₄ $\xrightarrow{442.0^{\circ}\text{C}}$ Rb₃BeF₅) were observed in the RbF-BeF₂ system. Little thermochemical information about the RbF-BeF₂ system has been reported to date. The RbF-BeF₂ system was optimized in this study based on the substitutional solution model using the experimental data from Moore et al. [21], because their data were more accurate than those of Grebenshchikov [46].

2.3 CsF-BeF₂ system

Only Breusov et al. [47] reported the phase equilibrium information of the CsF-BeF₂ system using thermal analysis. The CsF-BeF₂ system contains four intermediate compounds—Cs₃BeF₅, Cs₂BeF₄, CsBeF₃ and CsBe₂F₅—where Cs₂BeF₄, CsBeF₃, and CsBe₂F₅ were discovered to melt congruently at 793.0 °C, 475.0 °C, and 480.0 °C, respectively, but Cs₃BeF₅ melted incongruently at 659.0 °C. Four eutectic reactions (Liquid $\xrightarrow{598.0^{\circ}\text{C}}$ CsF + Cs₃BeF₅, Liquid $\xrightarrow{449.0^{\circ}\text{C}}$ Cs₂BeF₄ + CsBeF₃, Liquid $\xrightarrow{393.0^{\circ}\text{C}}$ CsBeF₃ + CsBe₂F₅, and Liquid $\xrightarrow{367.0^{\circ}\text{C}}$ CsBe₂F₅ + BeF₂) and one peritectic reaction (Liquid + Cs₂BeF₄ $\xrightarrow{659.0^{\circ}\text{C}}$ Cs₃BeF₅) were the distinct features of the CsF-BeF₂ system. Thermochemical data for the CsF-BeF₂ system are still lacking. Similar to the systems mentioned above, a substitutional solution model was used to optimize this system based on experimental data from Breusov et al. [41].

2.4 KF-CsF system

The phase diagram of the KF-CsF system was solely obtained by Samuseva et al. [53] through thermal analysis. This system is eutectic with one eutectic point located at 625.0 °C and 0.570 mol CsF. In addition, the limited solid solubility of KF in CsF is 0.15 mol at 625.0 °C. To date, few thermochemical studies of the KF-CsF system have been reported. A substitutional solution model was used to optimize the KF-CsF system based on experimental data from Samuseva et al. [53].

2.5 RbF-CsF system

The phase diagram of the RbF-CsF system was investigated by Samuseva et al. [53] and Beneš et al. [54] using thermal analysis. The phase diagram reported by Samuseva et al. [53] shows a temperature minimum for the solidus without a corresponding minimum for the liquidus, which violates the phase rule. The liquidus of the RbF-CsF system was optimized by Sangster and Pelton [55] based on the liquidus experimental data of Samuseva et al. However, there was a significant deviation between the calculated phase diagram and liquidus experimental data obtained by Samuseva et al.

Subsequently, new measurements of the solidus and liquidus equilibria of the RbF-CsF system were obtained by Beneš et al. [54]. The phase diagram of the RbF-CsF system was first constructed using a quasi-chemical model based on the measured experimental data, where the calculated phase diagram agreed well with the experimental values. In this study, the RbF-CsF system was calculated using the substitutional solution model to maintain the consistency of the model. The experimental data from Beneš et al. were used to optimize the RbF-CsF system in the present work.

2.6 KF-RbF system

The KF-RbF system is isomorphous with a minimum point in the liquidus curve, which was systematically evaluated and optimized by Yin et al. [56]. The thermodynamic parameters obtained in that study were directly adopted in the present work.

2.7 Sub-ternary systems

Little relevant information has been reported to date for the ternary KF-RbF-BeF₂, KF-CsF-BeF₂, RbF-CsF-BeF₂, and KF-RbF-CsF systems. These ternary systems were investigated in this study based on the thermodynamic parameters of the binary systems using model extrapolation.

3 Methods

3.1 Thermodynamic optimization

The PanOptimizer module included in the PANDAT software, which is a C/C++ software package for optimizing thermodynamics and thermophysical properties, was used to optimize the thermodynamic parameters. The weighted least-squares technique was adopted during the optimization process, and a trial-and-error method was used to regulate the optimization weight factor until the optimized value agreed well with the experimental phase equilibrium data and the theoretically calculated value.

Table 1 Thermodynamic parameters of the KF-RbF-CsF-BeF₂ system from FactSage 7.2

Compound	Gibbs energy (J)	Temp. (K)
KF (Solid)	$-581,701.002 + 245.661 T - 45.982 \ln(T) - 0.007 T^2$	298.15–2000
KF (Liquid)	$-567,937.997 + 372.694 T - 66.944 T \ln(T)$	298.15–2000
RbF (Solid)	$-563,090.817 + 158.256 T - 33.330 T \ln(T) - 0.019 T^2 - 251,040.000 T^{-1}$	298.15–1500
	$-558,571.051 + 313.921 T - 58.994 T \ln(T)$	1500–1663
RbF (Liquid)	$-546,097.480 + 300.480 T - 58.994 T \ln(T)$	298.15–1066
	$-297,259.229 - 607.417 T + 47.292 T \ln(T) - 0.002 T^2 - 73,360,164.000 T^{-1}$	1066–1200
	$-544,409.532 + 298.957 T - 58.994 T \ln(T)$	1200–1663
CsF (Solid)	$-569,380.712 + 229.686 T - 46.685 T \ln(T) - 0.009 T^2$	298.15–2000
CsF (Liquid)	$-565,929.140 + 405.902 T - 74.057 T \ln(T)$	298.15–2000
BeF ₂ (Solid)	$-1,041,405.769 + 271.945 T - 47.363 T \ln(T) - 0.017 T^2$	298.15–1300
	$-1,029,550.268 + 331.677 T - 60.000 T \ln(T)$	1300–1301
BeF ₂ (Liquid)	$-848,170.113 - 1703.462 T + 188.684 T \ln(T) - 1,415,912.346 T^{-1} - 5.801 T^{1.5} + 26,373.417 T^{0.5} - 74,606.149 \ln(T)$	298.15–2000
	$-990,282.352 + 304.240 T - 60.000 T \ln(T) - 0.010 T^2$	2000–2001

3.2 Thermodynamic model

3.2.1 Pure component

The Gibbs energy function of the pure component is described as follows, and the corresponding coefficients of the pure component are listed in Table 1:

$$^{\circ}G_i^{\phi}(T) = a + bT + cT \ln(T) + dT^2 + eT^3 + \frac{f}{T} + \sum_n g_n T^n \quad (1)$$

where a – f and g_n denote the corresponding coefficients, n refers to a set of integers, and T is the absolute temperature (K). The Gibbs free energy function of the pure components was adopted from the FactSage database.

3.2.2 Solution phase

The solution phase, that is, the liquid phase of the AF-BeF₂ ($A = K, Rb$, and Cs) and A'F-CsF ($A' = K$ and Rb) systems, and the solid solution phase of the A'F-CsF ($A' = K$ and Rb) system, were thermodynamically described using the substitutional solution model, where the Gibbs free energy is expressed as follows:

$$G_{AF-BeF_2}^{Liquid} = x_{AF} G_{AF}^{liq} + x_{BeF_2} G_{BeF_2}^{liq} + RT(x_{AF} \ln x_{AF} + x_{BeF_2} \ln x_{BeF_2}) + x_{AF} x_{BeF_2}^{\nu} L_{x_{AF} \rightarrow x_{BeF_2}}^{liq} (x_{AF} - x_{BeF_2})^{\nu} \quad (A = K, Rb \text{ and } Cs) \quad (2)$$

$$G_{A'F-CsF}^{Liquid} = x_{A'F} G_{A'F}^{liq} + x_{CsF} G_{CsF}^{liq} + RT(x_{A'F} \ln x_{A'F} + x_{CsF} \ln x_{CsF}) + x_{A'F} x_{CsF}^{\nu} L_{x_{A'F} \rightarrow x_{CsF}}^{liq} (x_{A'F} - x_{CsF})^{\nu} \quad (A' = K \text{ and } Rb) \quad (3)$$

where x_{AF} , x_{BeF_2} , $x_{A'F}$, and x_{CsF} are the mole fractions of AF, BeF₂, A'F, and CsF, respectively. G_{AF}^{liq} , $G_{BeF_2}^{liq}$, $G_{A'F}^{liq}$, and G_{CsF}^{liq} are the Gibbs free energies of AF, BeF₂, A'F, and CsF, respectively. L^{liq} is the interaction parameter for the AF-BeF₂ and A'F-CsF systems, which is a function of temperature [57].

3.2.3 Intermediate phase

The intermediate phases, that is, KBeF₃, K₂BeF₄, K₃BeF₅, KBe₂F₅, RbBeF₃, Rb₂BeF₄, Rb₃BeF₅, RbBe₂F₅, CsBeF₃, Cs₂BeF₄, Cs₃BeF₅, and CsBe₂F₅, were thermodynamically described by the compound energy formalism, in which the Gibbs free energy is expressed as follows:

$$G_{(AF)_x(BeF_2)_y}^{solid} = xG_{AF}^{\circ} + yG_{BeF_2}^{\circ} + \Delta_f H_{(AF)_x(BeF_2)_y}^{\circ} - T\Delta_f S_{(AF)_x(BeF_2)_y}^{\circ} \quad (4)$$

where G_{AF}° and $G_{BeF_2}^{\circ}$ denote the Gibbs energies of the pure component AF and BeF₂, respectively. $\Delta_f H_{(AF)_x(BeF_2)_y}^{\circ}$ and $\Delta_f S_{(AF)_x(BeF_2)_y}^{\circ}$ represent the formation enthalpy and entropy, respectively, of the intermediate phase (AF)_x(BeF₂)_y. $\Delta_f H_{(AF)_x(BeF_2)_y}^{\circ}$ was predicted based on density functional theory (DFT) and was used as the initial value of thermodynamic optimization for the corresponding AF-BeF₂ ($A = K, Rb$, and Cs) systems shown in Table 2.

3.3 Theoretical prediction of formation enthalpy

The formation enthalpies of the intermediate compounds ABeF₃, A₂BeF₄, A₃BeF₅, and ABe₂F₅ ($A = K, Rb$, and Cs) were predicted based on the Open Quantum Materials Database (OQMD), which is a high-throughput database includes many DFT energies of compounds. The formation enthalpy was used as the initial value to optimize the sub-binary systems of the KF-RbF-CsF-BeF₂ system. The relevant calculated equations of the formation enthalpy are as follows based on the DFT single-point energy of the corresponding compounds:

$$\Delta_f H_{ABeF_3} = E_{tot}(ABeF_3) - E_{tot}(AF) - E_{tot}(BeF_2) \quad (5)$$

$$\Delta_f H_{A_2BeF_4} = E_{tot}(A_2BeF_4) - 2E_{tot}(AF) - E_{tot}(BeF_2) \quad (6)$$

$$\Delta_f H_{A_3BeF_5} = E_{tot}(A_3BeF_5) - 3E_{tot}(AF) - E_{tot}(BeF_2) \quad (7)$$

Table 2 The single point energies of the compounds from the KF-RbF-CsF-BeF₂ system

Compd	E_{tot} (eV/atom)	E_{tot} (kJ/mol)	Compd	E_{tot} (eV/atom)	E_{tot} (kJ/mol)
KF	-5.822	-560.775	RbBeF ₃	-16.745	-1612.878
RbF	-5.710	-549.987	Rb ₂ BeF ₄	-22.911	-2206.787
CsF	-5.662	-545.364	Rb ₃ BeF ₅	-28.620	-2756.678
BeF ₂	-10.545	-1015.694	RbBe ₂ F ₅	-27.320	-2631.462
KBeF ₃	-16.780	-1616.250	CsBeF ₃	-16.825	-1620.584
K ₂ BeF ₄	-23.016	-2216.901	Cs ₂ BeF ₄	-22.932	-2208.810
K ₃ BeF ₅	-28.836	-2777.483	Cs ₃ BeF ₅	-28.593	-2754.078
KBe ₂ F ₅	-27.328	-2632.233	CsBe ₂ F ₅	-27.416	-2640.709

Table 3 Summary of the calculated thermodynamic parameters of the sub-binary systems of the KF-RbF-CsF-BeF₂ system

Systems	Phases	Models	Thermodynamic Parameters
KF-BeF ₂	Liquid	(KF, BeF ₂) _{1.0}	${}^0L_{\text{KF,BeF}_2}^{\text{Liquid}} = -84,718.8 + 10.910T$
			${}^1L_{\text{KF,BeF}_2}^{\text{Liquid}} = -37,828.8 + 25.000T$
			${}^2L_{\text{KF,BeF}_2}^{\text{Liquid}} = 21,813.6$
			$G_{\text{K}_3\text{BeF}_5} = 3G_{\text{KF}} + G_{\text{BeF}_2} - 67,039.2$
			$G_{\text{K}_2\text{BeF}_4} = 2G_{\text{KF}} + G_{\text{BeF}_2} - 40,000.0 - 23.063T$
RbF-BeF ₂	Liquid	(RbF, BeF ₂) _{1.0}	$G_{\text{KBeF}_3} = G_{\text{KF}} + G_{\text{BeF}_2} - 34,842.2$
			$G_{\text{KBe}_2\text{F}_3} = G_{\text{KF}} + 2G_{\text{BeF}_2} - 32,022.7 - 15.548T$
			${}^0L_{\text{RbF,BeF}_2}^{\text{Liquid}} = -106,785.0 + 6.637T$
			${}^1L_{\text{RbF,BeF}_2}^{\text{Liquid}} = -39,719.9 + 24.390T$
			${}^2L_{\text{RbF,BeF}_2}^{\text{Liquid}} = 29,064.2$
CsF-BeF ₂	Liquid	(CsF, BeF ₂) _{1.0}	$G_{\text{Rb}_3\text{BeF}_5} = 3G_{\text{RbF}} + G_{\text{BeF}_2} - 90,700.0$
			$G_{\text{Rb}_2\text{BeF}_4} = 2G_{\text{RbF}} + G_{\text{BeF}_2} - 61,540.0 - 23.017T$
			$G_{\text{RbBeF}_3} = G_{\text{RbF}} + G_{\text{BeF}_2} - 47,850.0 - 3.561T$
			$G_{\text{RbBe}_2\text{F}_3} = G_{\text{RbF}} + 2G_{\text{BeF}_2} - 53,400.0 - 14.334T$
			${}^0L_{\text{CsF,BeF}_2}^{\text{Liquid}} = -117,030.0 + 7.270T$
KF-CsF	Liquid	(KF, CsF) _{1.0}	${}^1L_{\text{CsF,BeF}_2}^{\text{Liquid}} = -36,015.8 + 20.374T$
			${}^2L_{\text{CsF,BeF}_2}^{\text{Liquid}} = 30,962.9$
			$G_{\text{Cs}_3\text{BeF}_5} = 3G_{\text{CsF}} + G_{\text{BeF}_2} - 98,868.7$
			$G_{\text{Cs}_2\text{BeF}_4} = 2G_{\text{CsF}} + G_{\text{BeF}_2} - 70,000.0 - 24.663T$
			$G_{\text{CsBeF}_3} = G_{\text{CsF}} + G_{\text{BeF}_2} - 54,730.0 - 5.700T$
RbF-CsF	Liquid	(RbF, CsF) _{1.0}	$G_{\text{CsBe}_2\text{F}_3} = G_{\text{CsF}} + 2G_{\text{BeF}_2} - 64,208.0 - 13.000T$
			${}^0L_{\text{KF,CsF}}^{\text{Liquid}} = 7,220.0 - 2.014T$
			${}^1L_{\text{KF,CsF}}^{\text{Liquid}} = -27,050.0 + 24.858T$
			${}^0L_{\text{Halite}}^{\text{Halite}} = 22,641.0 + 7.531T$
			${}^1L_{\text{Halite}}^{\text{Halite}} = 6,223.0 - 0.415T$
RbF-CsF	Liquid	(RbF, CsF) _{1.0}	${}^0L_{\text{RbF,CsF}}^{\text{Liquid}} = -20,438.8 + 15.102T$

L : Interaction parameter between the binary systems, expressed as $L = a + b \times T$ (T : temperature)

G : Gibbs free energy

$$\Delta_f H_{\text{ABe}_2\text{F}_5} = E_{\text{tot}}(\text{ABe}_2\text{F}_5) - E_{\text{tot}}(\text{AF}) - 2E_{\text{tot}}(\text{BeF}_2) \quad (8)$$

where $E_{\text{tot}}(\text{AF})$, $E_{\text{tot}}(\text{BeF}_2)$, $E_{\text{tot}}(\text{ABeF}_3)$, $E_{\text{tot}}(\text{A}_2\text{BeF}_4)$, $E_{\text{tot}}(\text{A}_3\text{BeF}_5)$, and $E_{\text{tot}}(\text{ABe}_2\text{F}_5)$ are the single points of AF, BeF₂, ABeF₃, A₂BeF₄, A₃BeF₅ and ABe₂F₅ (A = K, Rb, and Cs), respectively, as listed in Table 2.

3.4 AIMD

AIMD simulations were used to investigate the structure and properties of KF-RbF-CsF-BeF₂ systems with two different proportions (i.e., 3.50–28.92–21.78–45.80 mol% and 1.80–35.42–52.40–10.38 mol%), which are denoted as Mixtures 1 and 2, respectively, in the following sections. The initial simulation systems for the molten salts were constructed using a random insertion method, based on the densities predicted in the previous section. Mixtures 1 and 2 consisted of 140 atoms (2 K, 17 Rb, 12 Cs, 26 Be, and 83 F) and 118 atoms (1 K, 20 Rb, 29 Cs, 6 Be, and 62 F) atoms,

respectively. Because the temperature has little effect on the structure of molten salts [58], only the 650 °C was investigated in this study.

AIMD based on DFT was performed using the Vienna Ab initio Simulation Package [59–62]. The exchange–correlation energy was described using the Perdew–Burke–Ernzerhof functional of the generalized gradient approximation [63, 64]. The electron–ion core interactions were described by the projector-augmented plane-wave [65] method, and an energy cutoff of 600 eV for the plane-wave expansion of the wave functions was used. The Γ point was chosen to sample the Brillouin zone [66]. A time step of 1.0 fs and a simulation temperature of 650 °C were used for all AIMD simulations, and the convergence criterion for the total energy was set at 10^{−5} eV.

The simulation process was as follows. First, 5 ps simulations for the two systems were conducted in an NPT ensemble with a Langevin thermostat to optimize the cell volumes using the method of Parrinello and Rahman [67, 68]. The

corresponding equilibrium volumes were then obtained from the average of the last 3000 steps. Finally, 15 ps simulations for the two systems based on the equilibrium volumes were performed in an NVT ensemble with a Nosé thermostat [69, 70]. The systems reached equilibrium within 2 ps, and the structures and properties of the molten salt systems were obtained by analyzing the last 10,000 steps of the simulation.

The partial RDF is important for describing the atomic configuration in liquid systems and is defined as the probability of finding another atom at a distance r from a center reference atom, as shown in Eq. (9) [71]:

$$g_{ij}(r) = \frac{dn_j(r)}{4\pi r^2 \rho_j dr} \quad (9)$$

where Δn_j is the number of j atoms in the spherical shell between radii $r - 0.5\Delta r$ and $r + 0.5\Delta r$, i stands for the center atoms, and ρ_j is the atomic number density of element j in the system. In a molten salt system, the first shell CNs of the central atom can be obtained by integrating the RDF within the cutoff radius (R_{cut}), as expressed in Eq. (10) [71]:

$$CN_{ij} = \int_0^{R_{\text{cut}}} 4\pi r^2 \rho_j g_{ij}(r) dr \quad (10)$$

where R_{cut} is the radius corresponding to the first valley of the RDF. The ADF describes the three-body correlation information and is defined as the average of the angles between the central atom and any two adjacent coordinated atoms in the system, as shown in Eq. (11) [72]:

$$\theta_{jik} = \left\langle \cos^{-1} \frac{r_{ij}^2 + r_{ik}^2 - r_{jk}^2}{2r_{ij}r_{ik}} \right\rangle \quad (11)$$

Table 4 Formation enthalpies of the intermediate compounds from the sub-binary systems of KF-RbF-CsF-BeF₂ system in the present work and calculated values from the OQMD

Binary system	Compounds	OQMD (kJ/mol)	This work (kJ/mol)
KF-BeF ₂	K ₃ BeF ₅	-39.780	-67.039
	K ₂ BeF ₄	-79.656	-40.000
	KBeF ₃	-79.464	-34.842
	KBe ₂ F ₅	-40.069	-32.022
RbF-BeF ₂	Rb ₃ BeF ₅	-47.197	-90.700
	Rb ₂ BeF ₄	-91.119	-61.540
	RbBeF ₃	-91.022	-47.850
	RbBe ₂ F ₅	-50.086	-53.400
CsF-BeF ₂	Cs ₃ BeF ₅	-59.526	-98.868
	Cs ₂ BeF ₄	-102.388	-70.000
	CsBeF ₃	-102.292	-54.730
	CsBe ₂ F ₅	-63.956	-64.208

where j and k are the adjacent coordinated atoms within R_{cut} of central atom i . The self-diffusion coefficients can be used to depict the transport characteristics of the molten salt and reflect the diffusivity of each component in the molten salt. They can be calculated using the mean square displacement (MSD) and Einstein formula, according to Eqs. (12) and (13) [72]:

$$MSD_A(t) = \frac{1}{N_A} \sum_{i=1}^{N_A} |r_i(t) - r_i(0)|^2 \quad (12)$$

$$D_A = \lim_{t \rightarrow \infty} \frac{1}{6t} MSD_A(t) \quad (13)$$

where $r_i(t)$ is the displacement of an A-type atom at time t and N_A represents the total number of elements A.

4 Results and discussion

4.1 Binary system

All phase diagrams were plotted using the PanPhaseDiagram module of the PANDAT software based on the optimized thermodynamic parameters listed in Table 3. The calculated phase diagrams will be discussed in the following section. The optimized formation enthalpies of the intermediate compounds from the sub-binary systems of the KF-RbF-CsF-BeF₂ system and the calculated values from the OQMD are shown in Table 4. The calculated formation enthalpy agrees with most values from the OQMD, although some deviation between them exists owing to the different temperatures used (i.e., the values in the OQMD were obtained at 0 K, and the present optimized data were acquired at 298.15 K). Table 5 compares the calculated values of the key invariant points with the experimental data of the sub-binary systems of the KF-RbF-CsF-BeF₂ system.

Figures 1, 2, 3, 4 and 5 show the calculated phase diagrams of the AF-BeF₂ (A = K, Rb, and Cs) and A'F-CsF (A' = K and Rb) systems with the corresponding experimental data [21, 47, 53, 54]. As clearly observed from Fig. 1, the calculated value of the KF-BeF₂ system shows a high level of consistency with the experimental data from Moore et al., especially for the invariable point. For instance, the congruent melting temperatures of K₃BeF₅, K₂BeF₄, and KBe₂F₅ at 736.7 K, 784.7 K, and 357.1 K, respectively, are in excellent agreement with the experimental values of 740.0 K, 787.0 K, and 358.0 K, respectively [21]. As shown in Fig. 2, good agreement exists between the calculated values of the RbF-BeF₂ system and the experimental data from Moore et al., except for some small deviation in the liquidus of the BeF₂ end

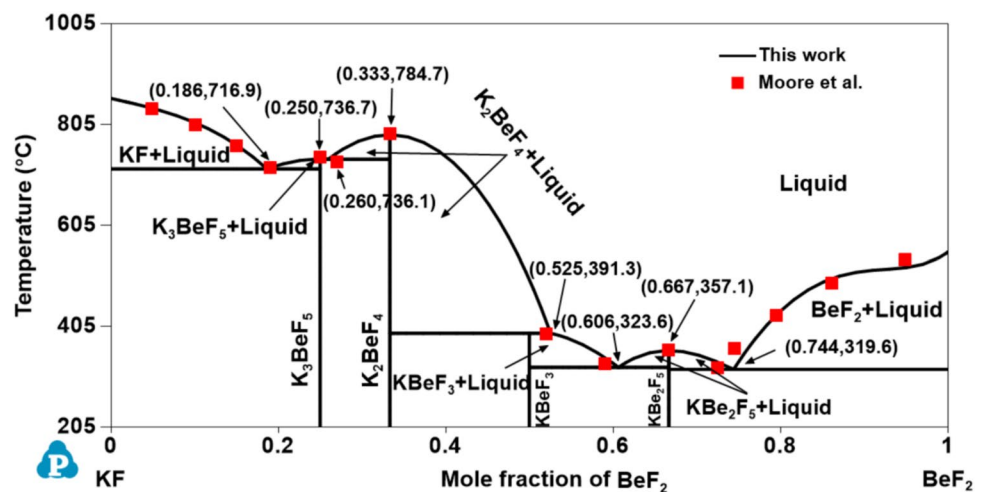
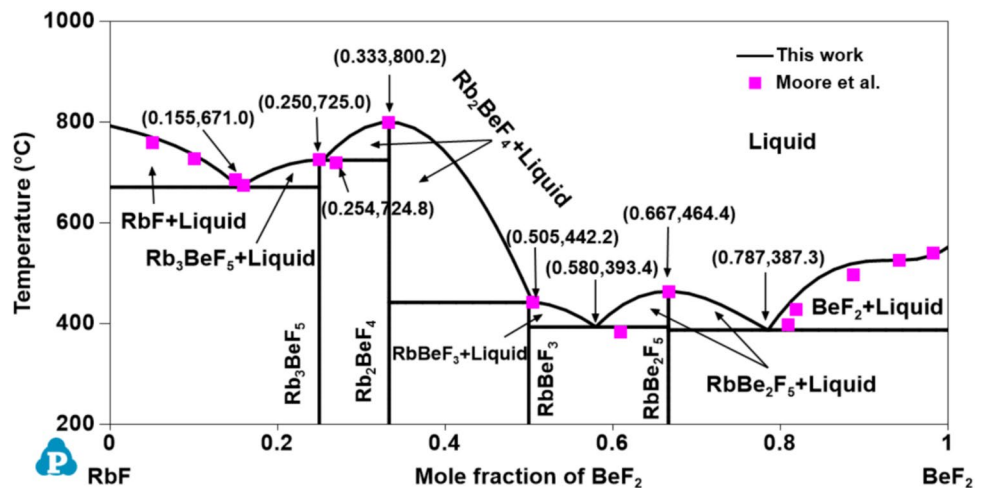
Table 5 Comparison between the calculated values of key points and experimental data of the sub-binary systems of the KF-RbF-CsF-BeF₂ system

System	Reaction	Invariant point		Reference
		T (°C)	χ_{BeF_2}	
KF-BeF ₂	Liquid \rightarrow K ₃ BeF ₅ + KF	716.8	0.186	[*]
		720.0	0.190	Moore et al
	Liquid \rightarrow K ₃ BeF ₅	736.7	0.250	[*]
		740.0	0.250	Moore et al
	Liquid \rightarrow K ₂ BeF ₄ + K ₃ BeF ₅	736.1	0.260	[*]
		730.0	0.270	Moore et al
	Liquid \rightarrow K ₂ BeF ₄	784.7	0.333	[*]
		787.0	0.333	Moore et al
	Liquid + K ₂ BeF ₄ \rightarrow KBeF ₃	391.3	0.525	[*]
		390.0	0.520	Moore et al
	Liquid \rightarrow KBeF ₃ + KBe ₂ F ₅	323.6	0.606	[*]
		330.0	0.590	Moore et al
	Liquid \rightarrow KBe ₂ F ₅	357.1	0.667	[*]
		358.0	0.667	Moore et al
	Liquid \rightarrow BeF ₂ + KBe ₂ F ₅	319.6	0.744	[*]
		323.0	0.725	Moore et al
RbF-BeF ₂	Reaction	T (°C)	χ_{BeF_2}	Reference
	Liquid \rightarrow RbF + Rb ₃ BeF ₅	671.0	0.155	[*]
		675.0	0.160	Moore et al
	Liquid \rightarrow K ₃ BeF ₅	725.0	0.250	[*]
		725.0	0.250	Moore et al
	Liquid \rightarrow Rb ₂ BeF ₄ + Rb ₃ BeF ₅	724.8	0.254	[*]
		720.0	0.270	Moore et al
	Liquid \rightarrow Rb ₂ BeF ₄	800.2	0.333	[*]
		800.0	0.333	Moore et al
	Liquid + Rb ₂ BeF ₄ \rightarrow RbBeF ₃	442.2	0.505	[*]
		442.0	0.505	Moore et al
	Liquid \rightarrow RbBeF ₃ + RbBe ₂ F ₅	393.4	0.580	[*]
		383.0	0.610	Moore et al
	Liquid \rightarrow RbBe ₂ F ₅	464.4	0.667	[*]
		464.0	0.667	Moore et al
	Liquid \rightarrow BeF ₂ + RbBe ₂ F ₅	387.3	0.787	[*]
		397.0	0.810	Moore et al
CsF-BeF ₂	Reaction	T (°C)	χ_{BeF_2}	Reference
	Liquid \rightarrow CsF + Cs ₃ BeF ₅	590.0	0.144	[*]
		598.0	0.140	Breusov et al
	Liquid + Cs ₂ BeF ₄ \rightarrow Cs ₃ BeF ₅	662.2	0.232	[*]
		659.0	0.235	Breusov et al
	Liquid \rightarrow Cs ₂ BeF ₄	793.0	0.333	[*]
		793.0	0.333	Breusov et al
	L \rightarrow CsBeF ₃ + Cs ₂ BeF ₄	459.8	0.479	[*]
		449.0	0.480	Breusov et al
	Liquid \rightarrow CsBeF ₃	465.0	0.500	[*]
		475.0	0.500	Breusov et al
	Liquid \rightarrow CsBeF ₃ + CsBe ₂ F ₅	388.7	0.582	[*]
		393.0	0.584	Breusov et al
	Liquid \rightarrow CsBe ₂ F ₅	480.0	0.667	[*]
		480.0	0.667	Breusov et al
	Liquid \rightarrow BeF ₂ + CsBe ₂ F ₅	362.5	0.792	[*]

Table 5 (continued)

System	Reaction	Invariant point		Reference
		T (°C)	χ_{BeF_2}	
KF-BeF ₂		367.0	0.775	Breusov et al
KF-CsF	Reaction	T (°C)	χ_{CsF}	Reference
	Liquid \rightarrow KF + (K,Cs)F	624.3	0.571	[*]
		625.0	0.570	Samuseva et al
	Halite \rightarrow (K,Cs)F#1 + (K,Cs)F#2	624.3	0.950	[*]
		625.0	0.850	Samuseva et al
RbF-CsF	Reaction	T (°C)	χ_{CsF}	Reference
	Liquid \rightarrow RbF + CsF	670.8	0.684	[*]
		673.85	0.726	Beneš et al
		677.85	0.750	Beneš et al

*: This work

Fig. 1 Calculated phase diagram of the KF-BeF₂ system with experimental data from Moore et al. (Color figure online)**Fig. 2** Calculated phase diagram of the RbF-BeF₂ system with experimental data from Moore et al. (Color figure online)

member. Similarly, the calculated melting temperatures of the intermediate phases Rb₃BeF₅, Rb₂BeF₄, and Rb₂BeF₄ at 725.0 K, 800.0 K, and 464.0 K, respectively, are nearly

equal to the experimental values of 725.0 K, 800.2 K, and 464.4 K, respectively [21]. As shown in Fig. 3, the calculated phase diagram of the CsF-BeF₂ system is in

Fig. 3 Calculated phase diagram of the CsF-BeF₂ system with experimental data from Breusov et al. (Color figure online)

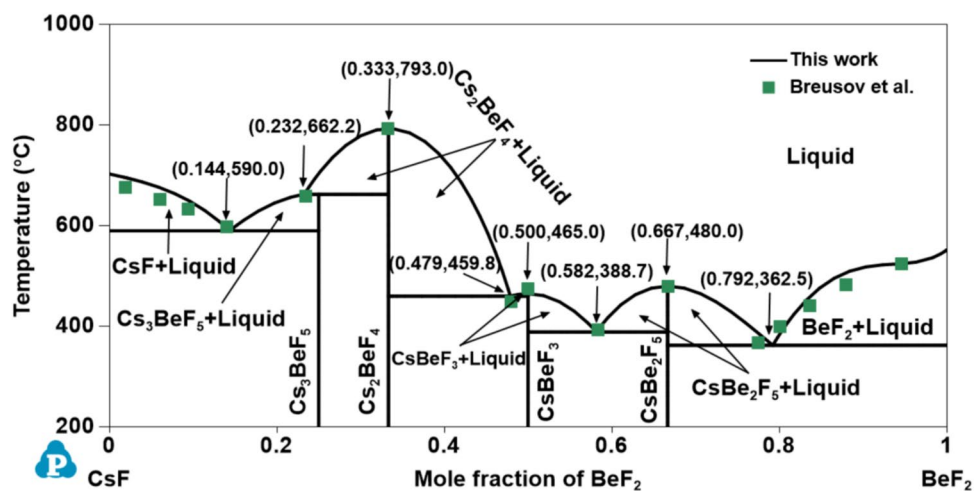


Fig. 4 Calculated phase diagram of the KF-CsF system with experimental data from Samuseva et al. (Color figure online)

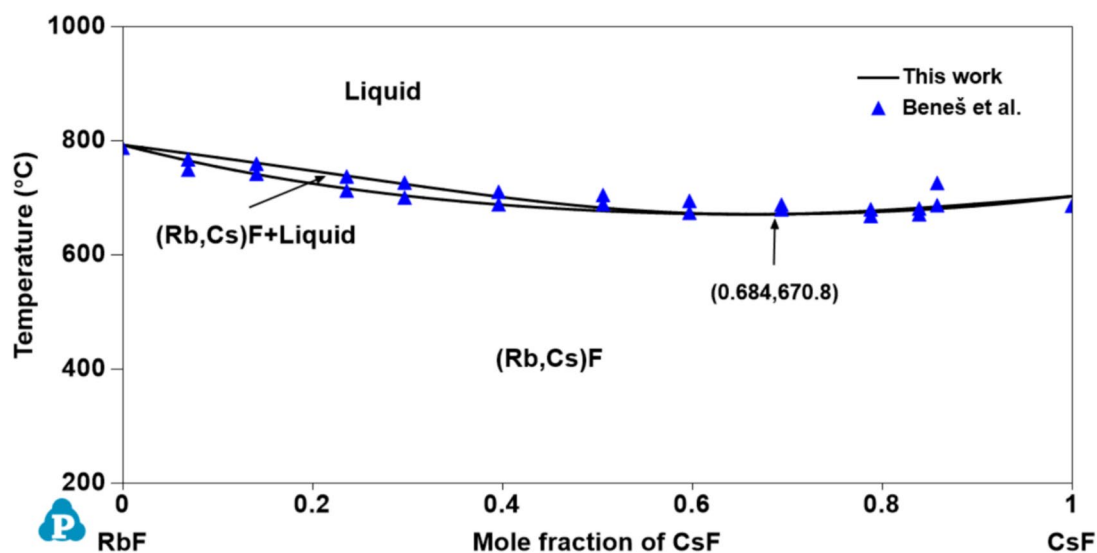
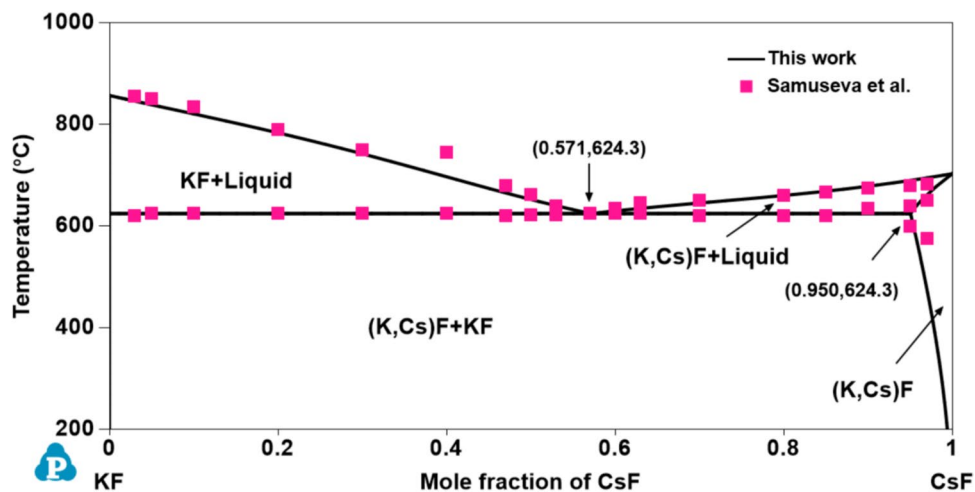


Fig. 5 Calculated phase diagram of the RbF-CsF system with experimental data from Beneš et al. (Color figure online)

good agreement with the experimental data from Breusov et al. [47], although some slight deviation is present on the rich-BeF₂ side. In particular, the calculated values of the key invariant points (i.e., 598.0 °C and 0.140 mol BeF₂, 793.0 °C and 0.333 mol BeF₂, and 480.0 °C and 0.667 mol BeF₂) are almost the same as the experimental data (590.0 °C and 0.144 mol BeF₂, 793.0 °C and 0.333 mol BeF₂, and 480.0 °C and 0.667 mol BeF₂), as shown in Table 5. As notably demonstrated by Fig. 4, the present calculated phase diagram of the KF-CsF system is in satisfactory agreement with the experimental data from Samuseva et al. [53], where the present calculated eutectic point of 624.3 °C and 0.571 mol CsF is almost the same as the experimental point of 625.0 °C and 0.570 mol CsF. The optimized solid solution point of 624.3 °C and 0.950 mol CsF also agrees well with the experimental point of 625.0 °C and 0.850 mol CsF. Figure 5 displays

the optimized phase diagram of the RbF-CsF system, where the optimized value corresponds well with the experimental data from Beneš et al. [54]. The present optimized minimum temperature on the liquidus (670.8 °C) agrees with the experimental results from Beneš et al. (677.85 °C and 673.85 °C).

4.2 Ternary system

The liquidus projections of the ternary BeF₂-KF-RbF, BeF₂-CsF-KF, BeF₂-CsF-RbF, and CsF-KF-RbF systems were calculated based on the thermodynamic parameters of the binary system using an extrapolation model. Figure 6(a–d) show the liquidus projections of these ternary systems with the primary phases and temperatures formed during the solidification process. In Fig. 6(d), no ternary invariant point is observed for the CsF-KF-RbF system

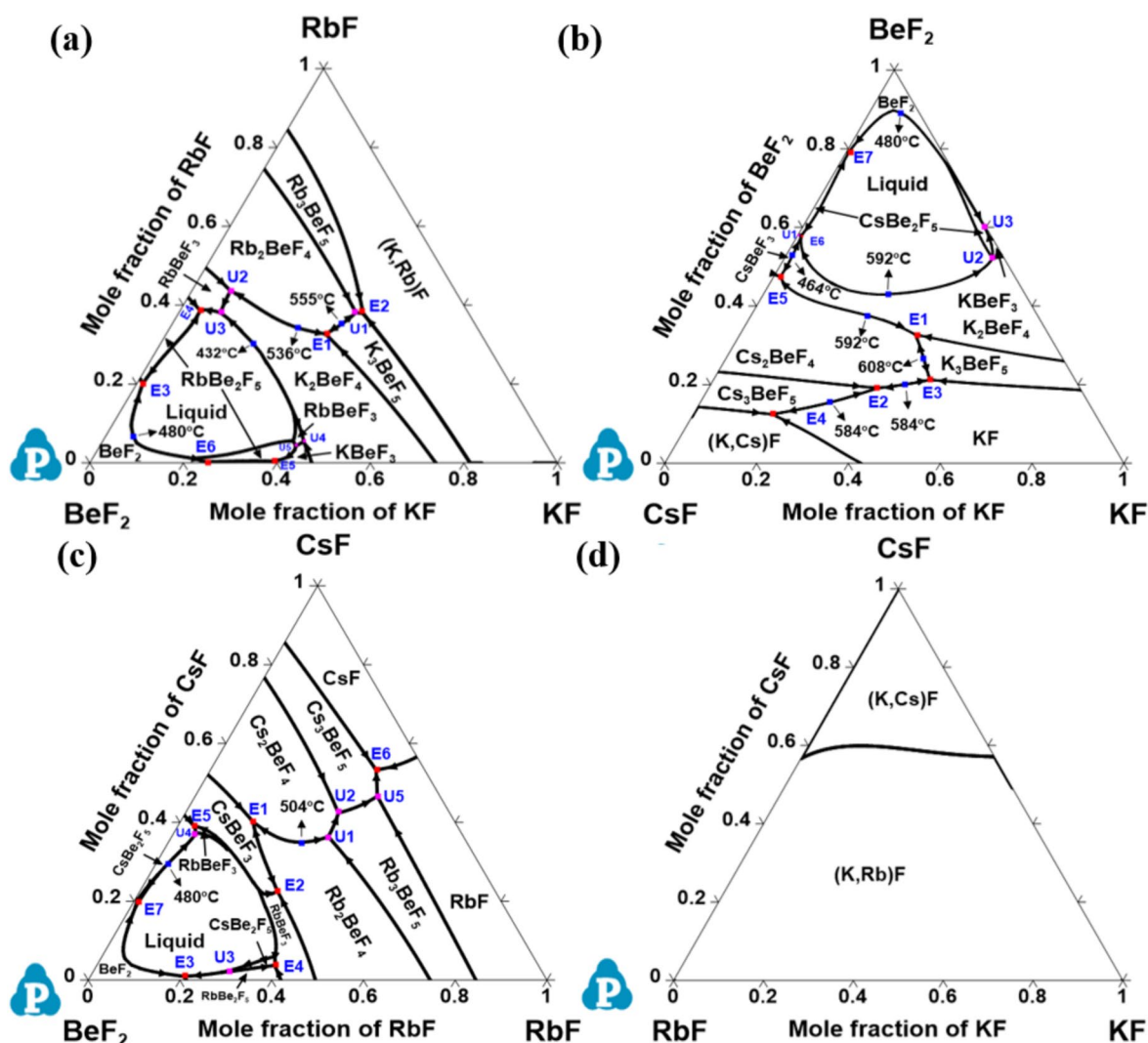


Fig. 6 (Color online) Calculated liquidus projections of the ternary (a) BeF₂-KF-RbF, (b) BeF₂-CsF-KF, (c) BeF₂-CsF-RbF, and (d) CsF-KF-RbF systems

Table 6 Calculated invariant reactions and temperatures of the BeF₂-KF-RbF, BeF₂-CsF-KF, BeF₂-CsF-RbF, and CsF-KF-RbF systems

Ternary system (A-B-C)	Reaction type	Temp. (°C)	χ_A	χ_B	χ_C
BeF ₂ -KF-RbF	Liquid $\xrightarrow{E1}$ K ₂ BeF ₄ + Rb ₂ BeF ₄ + K ₃ BeF ₅	537.7	0.3322	0.3405	0.3273
	Liquid + Rb ₂ BeF ₄ $\xrightarrow{U1}$ Rb ₃ BeF ₅ + K ₃ BeF ₅	529.1	0.2402	0.3786	0.3812
	Liquid $\xrightarrow{E2}$ (K, Rb)F + Rb ₃ BeF ₅ + K ₃ BeF ₅	526.8	0.2258	0.3950	0.3792
	Liquid + Rb ₂ BeF ₄ $\xrightarrow{U2}$ RbBeF ₃ + K ₂ BeF ₄	423.3	0.4809	0.0823	0.4368
	Liquid + K ₂ BeF ₄ $\xrightarrow{U3}$ RbBeF ₃ + Liquid	404.4	0.5298	0.0896	0.3806
	Liquid $\xrightarrow{E3}$ RbBe ₂ F ₅ + BeF ₂ + Liquid	382.3	0.7861	0.0128	0.2011
	Liquid $\xrightarrow{E4}$ RbBe ₂ F ₅ + RbBeF ₃ + Liquid	382.1	0.5703	0.0427	0.3870
	Liquid + K ₂ BeF ₄ $\xrightarrow{U4}$ RbBeF ₃ + KBeF ₃	378.0	0.5154	0.4309	0.0537
	Liquid + RbBeF ₃ $\xrightarrow{U5}$ RbBe ₂ F ₅ + KBeF ₃	371.4	0.5376	0.4193	0.0431
	Liquid $\xrightarrow{E5}$ RbBe ₂ F ₅ + KBeF ₃ + KBe ₂ F ₅	321.7	0.6064	0.3892	0.0044
	Liquid $\xrightarrow{E5}$ RbBe ₂ F ₅ + BeF ₂ + KBe ₂ F ₅	318.0	0.7442	0.2528	0.0030
BeF ₂ -CsF-KF	Liquid $\xrightarrow{E1}$ K ₂ BeF ₄ + Cs ₂ BeF ₄ + K ₃ BeF ₅	597.7	0.3276	0.2907	0.3817
	Liquid $\xrightarrow{E2}$ KF + Cs ₂ BeF ₄ + Cs ₃ BeF ₅	578.9	0.1917	0.4399	0.3684
	Liquid $\xrightarrow{E3}$ KF + Cs ₂ BeF ₄ + K ₃ BeF ₅	573.4	0.2126	0.3164	0.4710
	Liquid $\xrightarrow{E4}$ KF + Cs ₃ BeF ₅ + (K, Cs)F	553.3	0.1248	0.7035	0.1717
	Liquid $\xrightarrow{E5}$ K ₂ BeF ₄ + CsBeF ₅ + Cs ₂ BeF ₄	453.5	0.4746	0.5108	0.0146
	Liquid + K ₂ BeF ₄ $\xrightarrow{U1}$ CsBeF ₃ + Liquid	392.6	0.5189	0.0282	0.4529
	Liquid $\xrightarrow{E6}$ CsBeF ₃ + CsBe ₂ F ₅ + Liquid	385.0	0.5240	0.0253	0.4507
	Liquid + K ₂ BeF ₄ $\xrightarrow{U2}$ CsBeF ₃ + KBeF ₃	383.9	0.5214	0.0250	0.4536
	Liquid + CsBeF ₃ $\xrightarrow{U3}$ KBeF ₃ + CsBe ₂ F ₅	383.2	0.5239	0.0247	0.4514
	Liquid $\xrightarrow{E7}$ CsBe ₂ F ₅ + BeF ₂ + Liquid	359.8	0.7631	0.0056	0.2313
BeF ₂ -CsF-RbF	Liquid + Rb ₂ BeF ₄ $\xrightarrow{U1}$ Cs ₂ BeF ₄ + Rb ₃ BeF ₅	495.0	0.2946	0.3639	0.3415
	Liquid + Cs ₂ BeF ₄ $\xrightarrow{U2}$ Cs ₃ BeF ₅ + Rb ₃ BeF ₅	469.8	0.2428	0.4240	0.3332
	Liquid + CsBe ₂ F ₅ $\xrightarrow{U3}$ RbBe ₂ F ₅ + Liquid	446.2	0.7025	0.0191	0.2784
	Liquid $\xrightarrow{E1}$ Rb ₂ BeF ₄ + CsBeF ₃ + Cs ₂ BeF ₄	409.1	0.4399	0.4016	0.1585
	Liquid $\xrightarrow{E2}$ Rb ₂ BeF ₄ + RbBeF ₃ + CsBeF ₃	400.6	0.4746	0.2257	0.2997
	Liquid1 + Liquid2 $\xrightarrow{U4}$ CsBe ₂ F ₅ + RbBeF ₅	387.8	0.5635	0.0597	0.3768
	Liquid + Rb ₃ BeF ₅ $\xrightarrow{U5}$ Cs ₃ BeF ₅ + RbF	386.2	0.1366	0.4665	0.3969
	Liquid $\xrightarrow{E3}$ RbBe ₂ F ₅ + BeF ₂ + Liquid	383.4	0.7871	0.0098	0.2031
	Liquid $\xrightarrow{E4}$ CsBe ₂ F ₅ + RbBeF ₃ + RbBe ₂ F ₅	382.8	0.5745	0.0377	0.3878
	Liquid $\xrightarrow{E5}$ CsBe ₂ F ₅ + RbBeF ₃ + CsBeF ₃	374.9	0.5734	0.3894	0.0372
	Liquid $\xrightarrow{E6}$ Cs ₃ BeF ₅ + RbF + CsF	369.5	0.1057	0.5336	0.3607
	Liquid $\xrightarrow{E7}$ RbBe ₂ F ₅ + CsBe ₂ F ₅ + BeF ₂	359.4	0.7922	0.2018	0.0060
CsF-KF-RbF	Liquid + (K, Rb)F $\xrightarrow{U1}$ KF + (K, Cs)F	624.3	0.5716	0.4284	–
	(K, Rb)F + CsF $\xrightarrow{U2}$ Liquid + (K, Cs)F	450.0	0.5664	–	0.4336

because of the inherent properties of its sub-binary system, that is, KF-RbF and RbF-CsF are isomorphous systems with a minimum in the liquids. The BeF₂-KF-RbF system shown in Fig. 6(a) is characterized by six eutectic and five transition reactions, and the BeF₂-CsF-KF system features seven eutectic reactions and three transition reactions, as shown in Fig. 6(b). The BeF₂-CsF-RbF system is also characterized by seven eutectic reactions, but has five transition reactions, as depicted in Fig. 6(c). The results show that complex reactions can occur in the BeF₂-KF-RbF, BeF₂-CsF-KF, and BeF₂-CsF-RbF systems during the solidification process. The detailed invariant reactions and temperatures of the BeF₂-KF-RbF, BeF₂-CsF-KF, BeF₂-CsF-RbF, and CsF-KF-RbF systems are listed in Table 6.

4.3 Quaternary system

The quaternary KF-RbF-CsF-BeF₂ system was further investigated in terms of the thermodynamic databases of its sub-binary systems using an extrapolation model. The component proportions of the quaternary

KF-RbF-CsF-BeF₂ system were predicted based on its melting temperature. Table 7 shows the detailed melting point data with the corresponding component proportions; the melting temperature is not higher than 450.0 °C, which is a commonly acceptable temperature for the coolant in an MSR. As shown in Table 7, 10 kinds of KF-RbF-CsF-BeF₂ systems with different proportions were obtained through the thermodynamic calculations, where the content of BeF₂ varies from approximately 10 to 60 mol%. BeF₂-based molten salts commonly have much higher viscosities when the BeF₂ content of the molten salt is high (especially when the BeF₂ content is greater than 50 mol%). Therefore, the proportion of BeF₂ should be maintained within an acceptable range for practical applications. Thus, the quaternary KF-RbF-CsF-BeF₂ systems labeled No. (1)–(9) were chosen as relatively appropriate heat transfer media for MSRs based on the melting temperature ($T_{m.p.} \leq 450$ °C) and viscosity (i.e., BeF₂ content ≤ 50 mol%). The local structures of the KF-RbF-CsF-BeF₂ molten salts with different portions will be

Table 7 Predicted melting temperature (i.e., $T_{m.p.} \leq 450$ °C) with corresponding component proportions of the quaternary KF-RbF-CsF-BeF₂ system

Ternary system (A-B-C)	No.	Temp. (°C)	χ_A	χ_B	χ_C	χ_D
KF-RbF-CsF-BeF ₂	(1)	450.0	0.0180	0.3542	0.5240	0.1038
	(2)	450.0	0.3814	0.0043	0.0200	0.5943
	(3)	450.0	0.0200	0.0365	0.3816	0.5619
	(4)	378.7	0.0102	0.0368	0.3854	0.5676
	(5)	394.0	0.0806	0.3565	0.0347	0.5282
	(6)	450.0	0.1665	0.3232	0.0314	0.4789
	(7)	450.0	0.0327	0.1533	0.3885	0.4255
	(8)	431.5	0.0257	0.1544	0.3913	0.4286
	(9)	402.6	0.0350	0.2892	0.2178	0.4580
	(10)	450.0	0.0658	0.2800	0.2108	0.4434

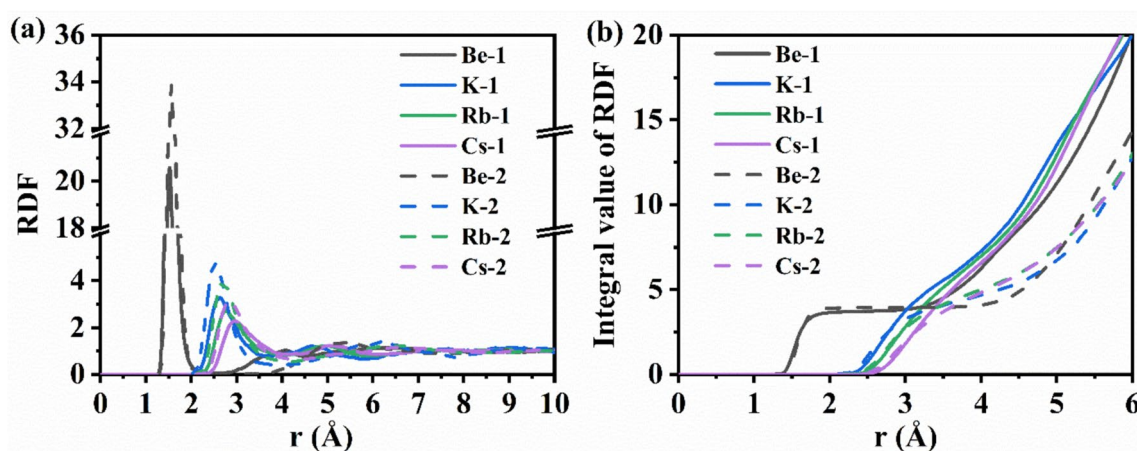


Fig. 7 (a) RDFs of Be-F, K-F, Rb-F, and Cs-F pairs, and (b) their corresponding integral curves. The solid and dashed lines represent the cases of Mixtures 1 and 2, respectively. (Color Figure online)

further discussed based on first-principles calculations in the following section.

4.3.1 RDFs

In the AIMD calculations, the NPT ensemble simulations revealed that the equilibrium densities of Mixture 1 (KF-RbF-CsF-BeF₂, 3.50–28.92–21.78–45.80 mol%) and Mixture 2 (KF-RbF-CsF-BeF₂, 1.80–35.42–52.40–10.38 mol%) at 650 °C were 2.22 g/cm³ and 2.72 g/cm³, respectively. Figure 7(a) presents the RDFs of the Be-F, K-F, Rb-F, and Cs-F ion pairs in the two molten salt systems. These systems exhibit some similar features. The RDFs for all cation–anion pairs have sharper and stronger first peaks, indicating an ordered arrangement of F[−] around Be²⁺, K⁺, Rb⁺, and Cs⁺. As the distance increases, the fluctuations of the RDFs gradually decrease and tend towards 1, reflecting the short-range order and long-range disorder in the microstructure of the molten salt systems. The highest first peak is observed for the Be-F ion pair, with the peak valley being almost zero, indicating a strong interaction between Be²⁺ and F[−]. This finding suggests that F[−] has more difficulty escaping from the coordination shell of Be²⁺ compared to those of other cations. The relative interaction strength of the cations with F[−] in the same system can be inferred from the heights of the first peaks for each ion pair as follows: Be²⁺ > K⁺ > Rb⁺ > Cs⁺. This correlates with the average

charge of the cations, and a higher charge results in stronger interactions with F[−]. Be²⁺ has the highest valence state and the smallest ionic radius among the cations, resulting in the strongest interaction. K⁺, Rb⁺, and Cs⁺ have the same valence state, and their interaction strength with F[−] decreases with increasing ionic radius: Cs⁺ > Rb⁺ > K⁺.

The first peak of the RDF of each ion pair in Mixture 1 is lower than that in Mixture 2, indicating a more ordered arrangement of F[−] around the cations in Mixture 2. The first peak position of the RDF typically represents the average bond length of the ion pair (Table 8). The peak positions of Be-F, K-F, Rb-F, and Cs-F in Mixture 1 are 1.55, 2.63, 2.77, and 2.95, respectively, and 1.57, 2.51, 2.69, and 2.83 in Mixture 2. With decreasing Be²⁺ content in Mixture 2, the average bond length of the Be-F ion pairs remains relatively unchanged, which is attributed to the strong interaction between Be²⁺ and F[−]. The Be–F bond length is almost the same as that in the LiF-BeF₂ system [48]. The peak positions for the other cation–anion pairs decrease significantly in Mixture 2 compared to those in Mixture 1. The bond length also reflects the strength of the ion pairs; shorter bond lengths indicate stronger interactions between the same ion pairs. Thus, the interactions between the cations and F[−] in Mixture 2 are stronger than those in Mixture 1. Because the concentration of Be²⁺ is higher in Mixture 1, F[−] preferentially binds with Be²⁺, thereby weakening its interactions with the other cations.

Table 8 First peak position and cutoff radius (R_{cut}) of the RDF (Å) and CNs of cations

	Mixture 1			Mixture 2		
	First peak	R_{cut}	CNs	First peak	R_{cut}	CNs
Be-F	1.55	2.45	3.72	1.57	2.43	3.93
K-F	2.63	3.69	6.14	2.51	3.61	4.23
Rb-F	2.77	3.97	6.73	2.69	3.93	4.89
Cs-F	2.95	4.11	7.03	2.83	4.09	5.01

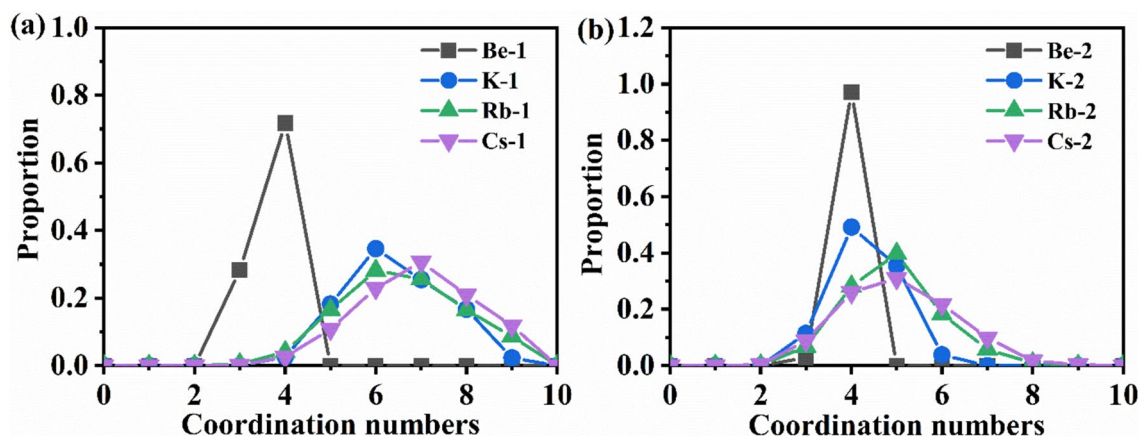


Fig. 8 Proportions of CNs in **a** Mixture 1 and **b** Mixture 2. (Color figure online)

4.3.2 CNs

The CNs were obtained by integrating the RDFs of the ion pairs. Figure 7(b) shows the integral values of the RDF for the Be-F, K-F, Rb-F, and Cs-F pairs in the two molten salt systems. In general, the values corresponding to R_{cut} in Fig. 7(b) are the CNs, and the calculated CNs for each cation are listed in Table 6. In Mixture 1, the CNs of Be²⁺, K⁺, Rb⁺, and Cs⁺ are 3.72, 6.14, 6.73, and 7.03, respectively, and in Mixture 2, they are 3.93, 4.23, 4.89, and 5.01, respectively. Except for Be²⁺, the CNs of the other cations in Mixture 1 are larger than those in Mixture 2, which is mainly owing to the higher concentration of F[−] in Mixture 1. Additionally, for the K-F, Rb-F, and Cs-F ion pairs, the integral curves do not exhibit a clear plateau near R_{cut} , as is present for the Be-F pair. Therefore, these cations can localize F[−] within a certain range, but there are no compact complex structures as Be²⁺. Furthermore, the proportions of CNs for all cations within the R_{cut} were calculated to study the coordination preference with F[−], as shown in Fig. 8. Be²⁺ predominantly forms fourfold coordination structures in both systems, like in the LiF-BeF₂ system, where Be²⁺ is dominated by [BeF₄]^{2−} [48]. For the K-F, Rb-F, and Cs-F ion pairs, the coordinated structures in their first coordination shells range from twofold to ninefold. The sixfold and sevenfold coordination structures account for the largest two portions in Mixture 1, whereas the fourfold and fivefold structures account for the largest portions in Mixture 2.

4.3.3 ADFs

To describe the three-body correlations of the ions in the molten salt systems further, the ADFs of F-Be-F, F-K-F, F-Rb-F, and F-Cs-F were calculated, as shown in Fig. 9. The angle of F-Be-F is mainly distributed in the range of 90°–130° both in Mixtures 1 and 2, with the maximum peak at approximately 109°. This corresponds to the slightly

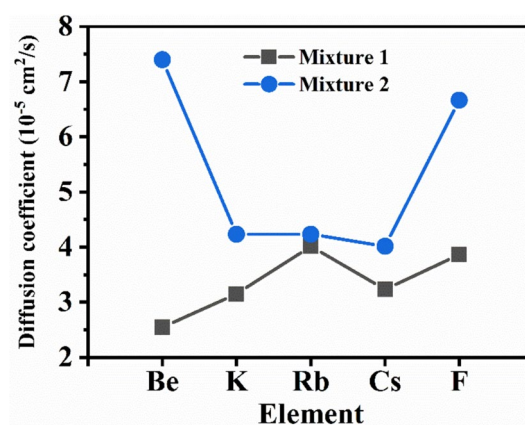


Fig. 10 Diffusion coefficients of the ions in two molten salt systems at 650 °C. (Color figure online)

distorted tetrahedral [BeF₄]^{2−}, consistent with that in the LiF-BeF₂ system [1]. For the F-K-F, F-Rb-F, and F-Cs-F pairs, the angle distribution range is wide and different from that for the F-Be-F pair in both Mixtures 1 and 2, and various coordination structures ranging from twofold to ninefold exist, as shown in Fig. 9. This is because K⁺, Rb⁺, and Cs⁺ do not form compact ion structures with F[−].

4.3.4 Diffusion coefficient

The diffusion coefficients of the ions were calculated using Eqs. (12) and (13), as illustrated in Fig. 10. The diffusion coefficients of Be²⁺, K⁺, Rb⁺, Cs⁺, and F[−] in Mixture 2 are 7.4×10^{-5} , 4.23×10^{-5} , 4.23×10^{-5} , 4.01×10^{-5} , and 6.67×10^{-5} cm²/s, respectively. Owing to their small ionic radii and masses, Be²⁺ and F[−] exhibit higher mobilities than the other ions. Conversely, characterized by its larger ionic radius and mass, Cs⁺ exhibits the lowest diffusion coefficient. As the proportion of BeF₂ increases in

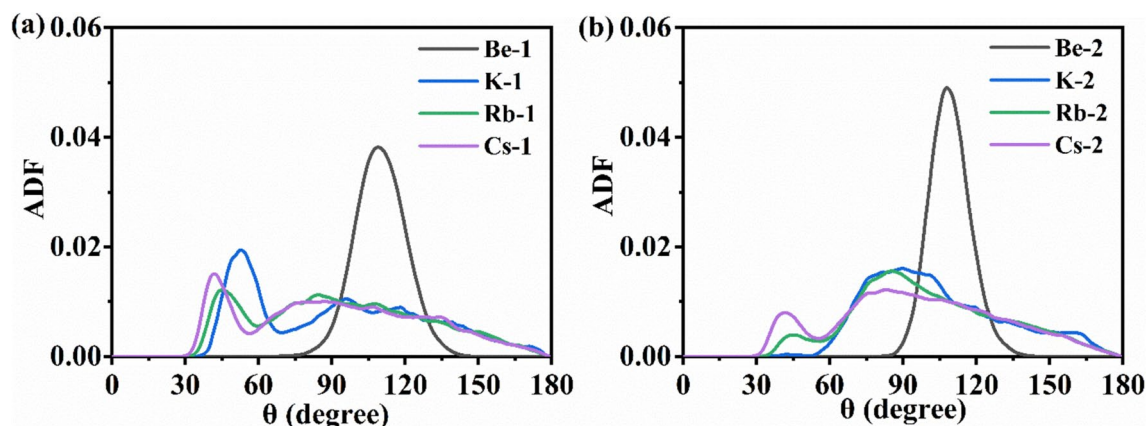


Fig. 9 ADFs of F-Be-F, F-K-F, F-Rb-F, and F-Cs-F in a Mixture 1 and b Mixture 2. (Color figure online)

Mixture 1, the diffusion coefficients of Be^{2+} , K^+ , Rb^+ , Cs^+ , and F^- decrease to 2.55×10^{-5} , 3.15×10^{-5} , 4.02×10^{-5} , 3.23×10^{-5} , and $3.87 \times 10^{-5} \text{ cm}^2/\text{s}$, respectively. Reflecting on the structural characteristics of the two systems, the binding strength between the same ion pair in Mixture 2 is stronger than that in Mixture 1, but the interactions between Be^{2+} and F^- significantly influence the overall stability of the system. Because the concentration of Be^{2+} in Mixture 1 is considerably higher than that in Mixture 2, it is more likely to form larger clusters between Be^{2+} and F^- . This can obviously reduce the diffusion coefficients of all ions in Mixture 1, especially Be^{2+} and F^- .

5 Conclusion

The binary (KF-BeF_2 , RbF-BeF_2 , CsF-BeF_2 , KF-CsF , and RbF-CsF), ternary ($\text{BeF}_2\text{-KF-RbF}$, $\text{BeF}_2\text{-CsF-KF}$, $\text{BeF}_2\text{-CsF-RbF}$, and CsF-KF-RbF), and quaternary KF-RbF-CsF-BeF_2 systems were thermodynamically calculated using the CALPHAD technique. Furthermore, the RDFs, CNs, ADFs, and diffusion coefficients of the quaternary KF-RbF-CsF-BeF_2 system were calculated using AIMD. The main contributions of this work are as follows:

- (1) A set of self-consistent and reliable thermodynamic databases for the KF-BeF_2 , RbF-BeF_2 , CsF-BeF_2 , KF-CsF , and RbF-CsF systems was established.
- (2) The liquidus projections and invariant points of $\text{BeF}_2\text{-KF-RbF}$, $\text{BeF}_2\text{-CsF-KF}$, $\text{BeF}_2\text{-CsF-RbF}$, and CsF-KF-RbF systems were obtained.
- (3) The melting temperatures ($T_{\text{m.p.}} \leq 450 \text{ }^\circ\text{C}$) for quaternary KF-RbF-CsF-BeF_2 systems with different compositions were obtained.
- (4) The interaction strength between cations and anions in the system followed the order $\text{Be-F} > \text{K-F} > \text{Rb-F} > \text{Cs-F}$. The CNs of all cations were determined.
- (5) A high Be^{2+} concentration can reduce the diffusion coefficients of the ions, especially Be^{2+} and F^- .

The present study is the first of its type, to the best of our knowledge, and the results show that the quaternary KF-RbF-CsF-BeF_2 system with the proportion 3.50–28.92–21.78–45.80 mol% or 1.80–35.42–52.40–10.38 mol% is one of the most promising candidate coolants for MSR in terms of thermodynamics (i.e., $T_{\text{m.p.}} \leq 450 \text{ }^\circ\text{C}$ with appropriate viscosity) and kinetics (i.e., suitable local structure and diffusion coefficient). This work not only drastically enriches the databases of molten salts, but also provides direct guidelines for screening and optimizing molten salts in the nuclear energy field.

Author contributions All authors contributed to the study conception and design. Material preparation, data collection and analysis were performed by Hui-qin Yin, Lin-Bin Jiang, Xu-Chun Wu, Biao-Hu, Yang Wang and Wen-Guan Liu. The first draft of the manuscript was written by Hui-Qin Yin and all authors commented on previous versions of the manuscript. All authors read and approved the final manuscript.

Data availability The data that support the findings of this study are openly available in Science Data Bank at <https://cstr.cn/31253.11.sciencedb.j00186.00731> and <https://doi.org/10.57760/sciencedb.j00186.00731>.

Declarations

Conflict of interest The authors declare that they have no competing interests.

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